

Introduction

Biological nitrogen removal is the most commonly used system for the treatment of municipal wastewater.

Nitrification: $\text{NH}_4 \rightarrow \text{NO}_2$ Ammonia-Oxidizing bacteria
 $\text{NO}_2 \rightarrow \text{NO}_3$ Nitrite-Oxidizing bacteria
 Denitrification: $\text{NO}_2, \text{NO}_3 \rightarrow \text{N}_2$ Denitrifying bacteria

However, wastewater containing high salinity is known to significantly reduce the nitrification efficiency.

Background

The maximum acceptable salt range have a wide range (2.5-5%)
 The effect of salt on nitrification does not give a clear answer.

Target

The maximum acceptable salt range by immobilized microgram using entrapped and attached methods
 The effect of salt on nitrification activity

Materials and methods

Experimental equipment and operating method

Experimental equipment consists three reactors; nitrification tank, denitrification tank, Oxidic tank (Fig.1). The Influent (Inf) water flow in order nitrification tank to denitrification tank. The water of oxidic tank discharged as effluent (Eff) water. Air was supplied nitrification tank and oxidic tank. 3% Methanol was add as hydrogen donor in the denitrification tank. The oxidic tank removed methanol.

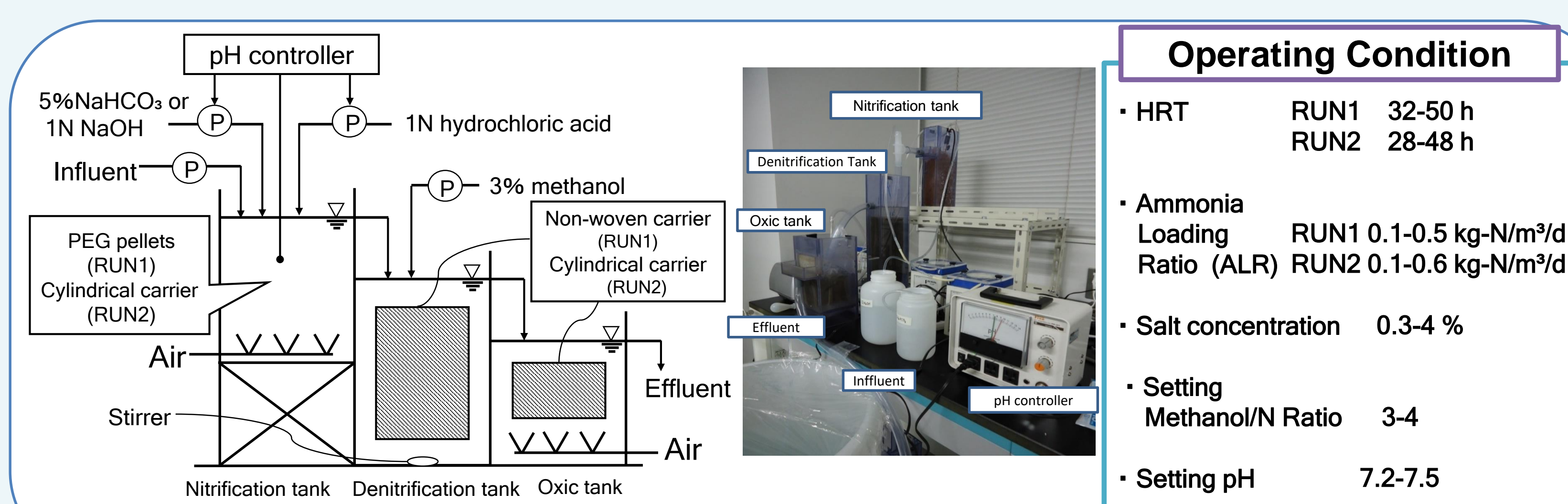


Fig.1 Beaker-scare reactors for evaluation of nitrification.

Wastewater

Inf water was an industrial wastewater generated from recovered rare metals. The wastewater had the following composition: $\text{NH}_4\text{-N}$ 90-1510 mg/L, NaHCO_3 3.0 g/L, $\text{Na}_2\text{HPO}_4 \cdot 12\text{H}_2\text{O}$ 0.25 g/L, 0.3-4% salt concentrations (mostly NaCl).

Pellets

RUN1 used immobilized microgram using entrapped pellets and attached carriers (Table 1, Fig.2). RUN2 used immobilized microgram using attached carrier and add an activated sludge.

Table 1 Pellets in each reactor

Reactor	Pellets
Nitrification tank	PEG pellet (Entrapped)*1
RUN1 Denitrification tank	Non-woven carrier (Attached)
Oxidic tank	Non-woven carrier (Attached)
Nitrification tank	Cylindrical carrier (Attached)
RUN2 Denitrification tank	Cylindrical carrier (Attached)
Oxidic tank	Cylindrical carrier (Attached)

* 1) Most Probable Number of Nitrification pellets

AH strain 4.10×10^8 cells/cm³ (98%)
 AL strain 6.56×10^6 cells/cm³ (2%)

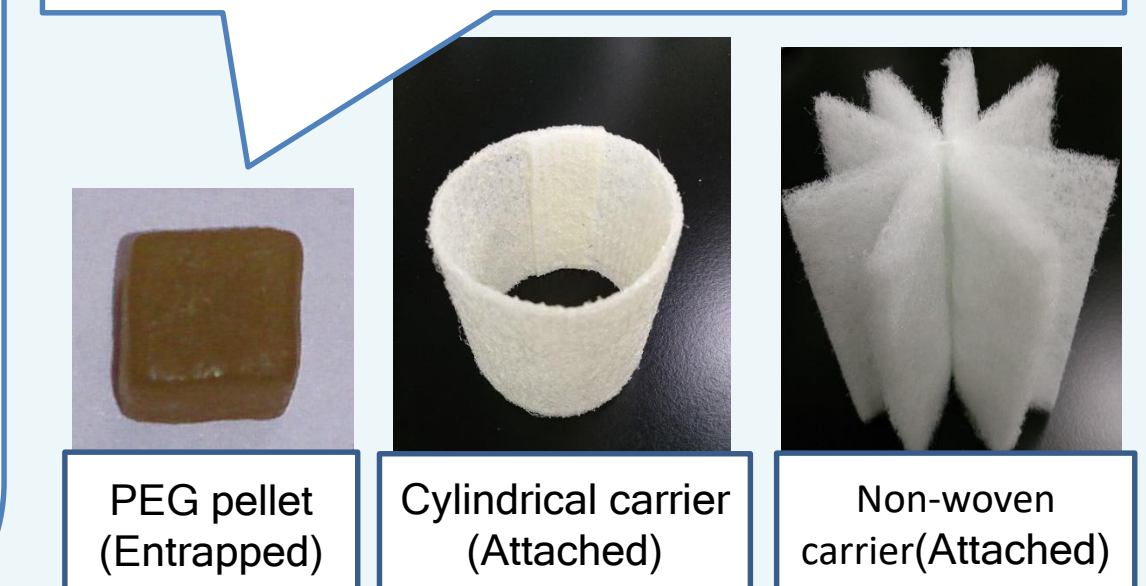


Fig.2 Used Pellets

Results and discussion

RUN1 (Immobilized microgram using entrapped method)

RUN1 increased salt concentration in the Inf water from 160 day. Nitrification rate was obtained $0.31 \text{ kg-N/m}^3/\text{d}$ and Eff T-N was obtained $<2.1 \text{ mg/L}$ under 3.8% salt concentrations (Fig3, 5).

Under 4% salt concentrations, nitrification rate decreased and $\text{NH}_4\text{-N}$ and $\text{NO}_2\text{-N}$ increased in the nitrification tank. From 380 day, RUN1 diluted 0.3 salt concentration. Nitrification activity recovered and nitrification rate was obtained $0.4 \text{ kg-N/m}^3/\text{d}$ and Eff T-N was obtained $<10.0 \text{ mg/L}$ again.

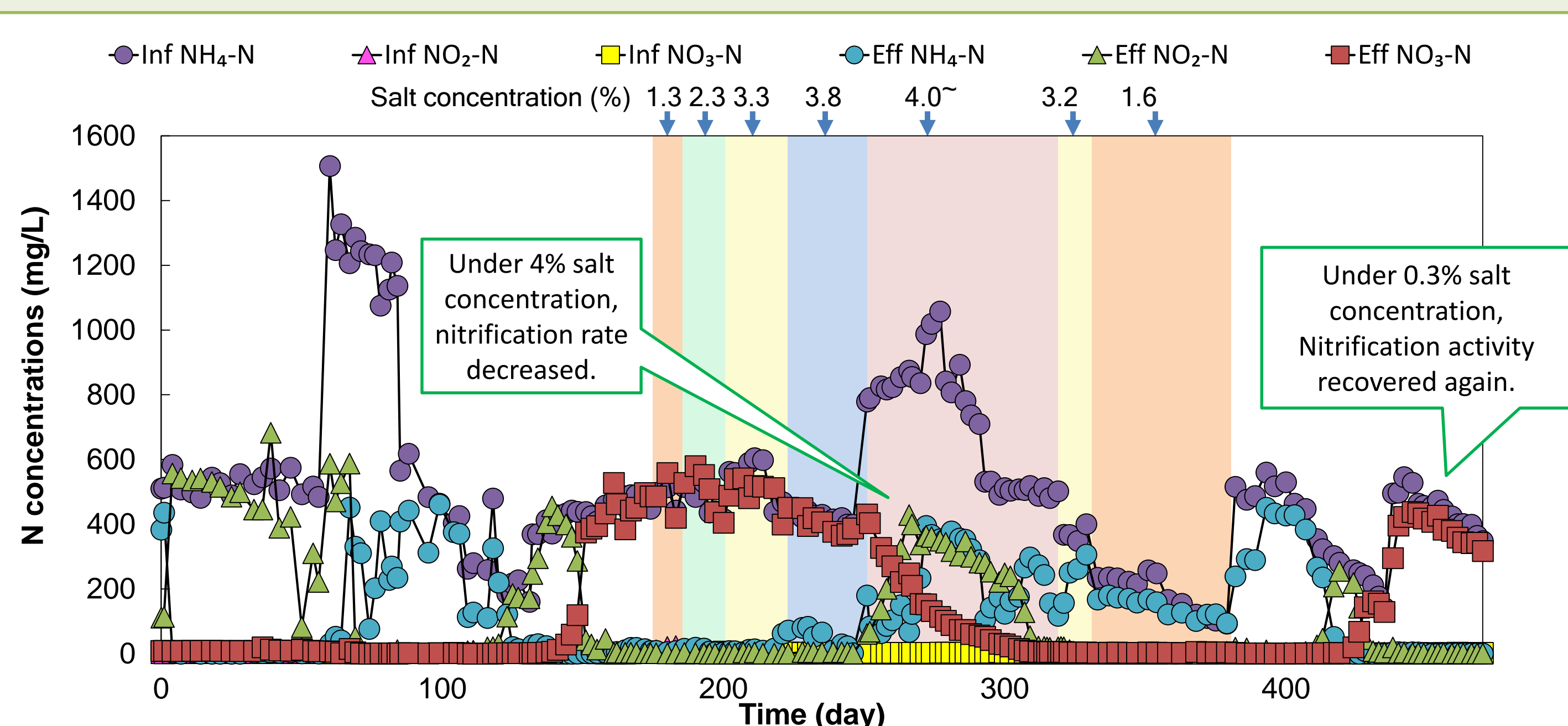


Fig.3 Nitrification performance under different salt concentrations (RUN1:Entrapped method, Nitrification tank)

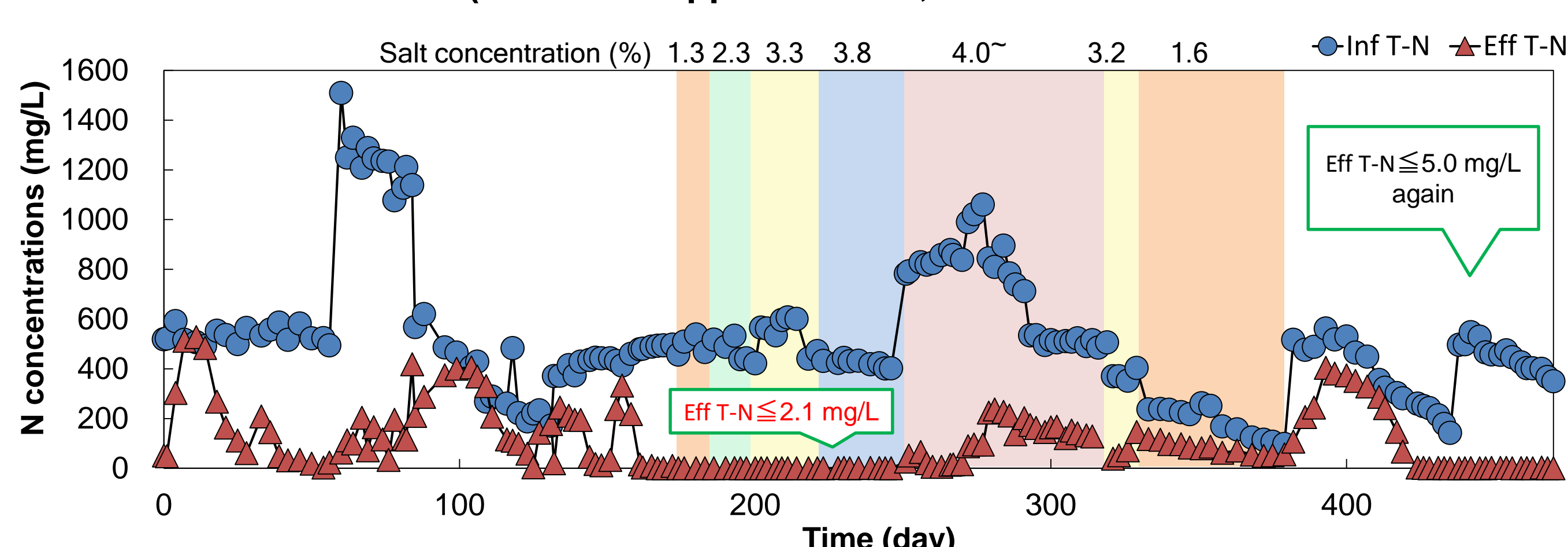


Fig.5 Total-N under different salt concentrations (RUN1:Entrapped method, Oxidic tank)

RUN2 (Immobilized microgram using attached method)

RUN2 increased salt concentration in the Inf water from 120 day. Nitrification rate was obtained $0.29 \text{ kg-N/m}^3/\text{d}$ and Eff T-N was obtained $<5.0 \text{ mg/L}$ under 3.8% salt concentrations (Fig4, 6).

Under 4% salt concentrations, nitrification rate was decreased and, $\text{NH}_4\text{-N}$ was increased in the nitrification tank. From 310 day, RUN2 diluted 0.3% salt concentration in the Inf water. Nitrification activity recovered. Nitrification rate was obtained $0.4 \text{ kg-N/m}^3/\text{d}$ and Eff T-N was obtained $<5.0 \text{ mg/L}$ again under 3.8% salt concentrations.

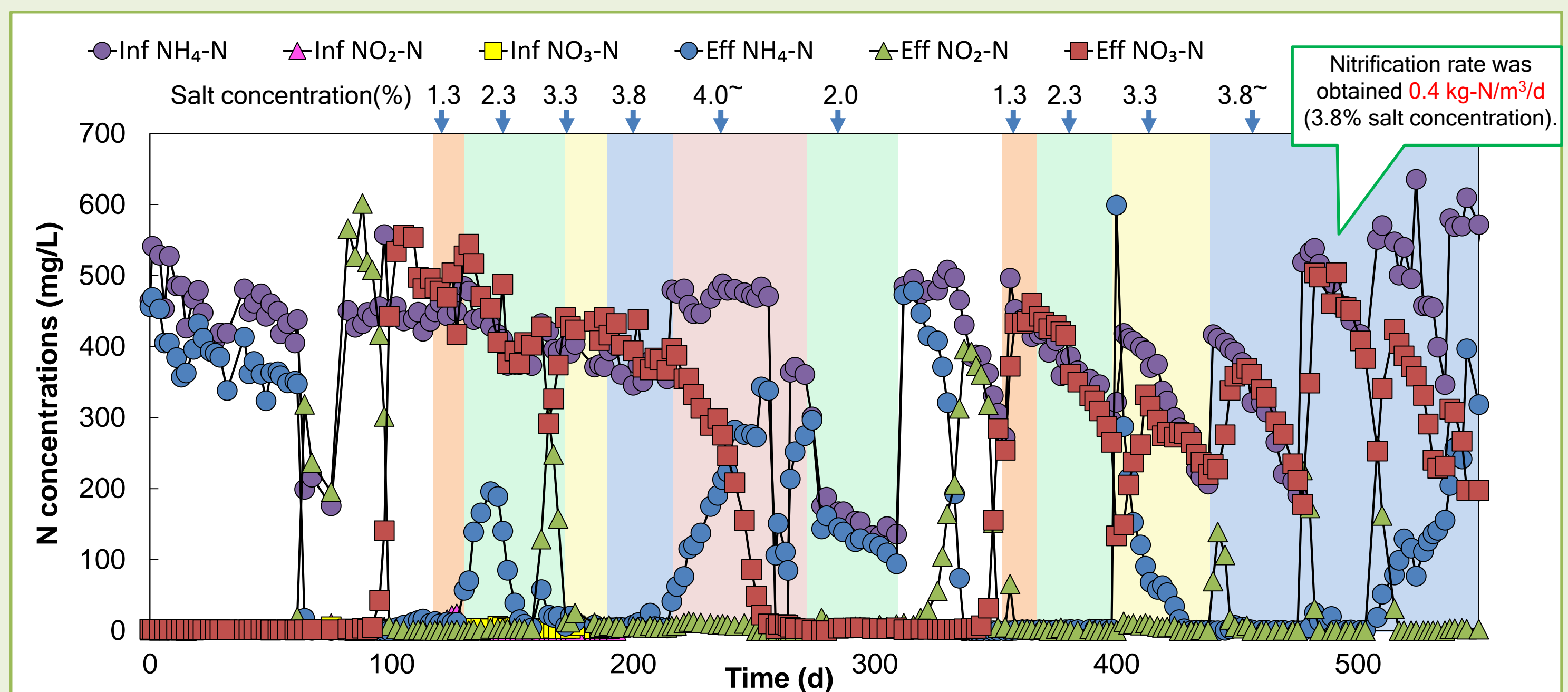


Fig.4 Nitrification performance under different salt concentrations (RUN2:Attached method, Nitrification tank)

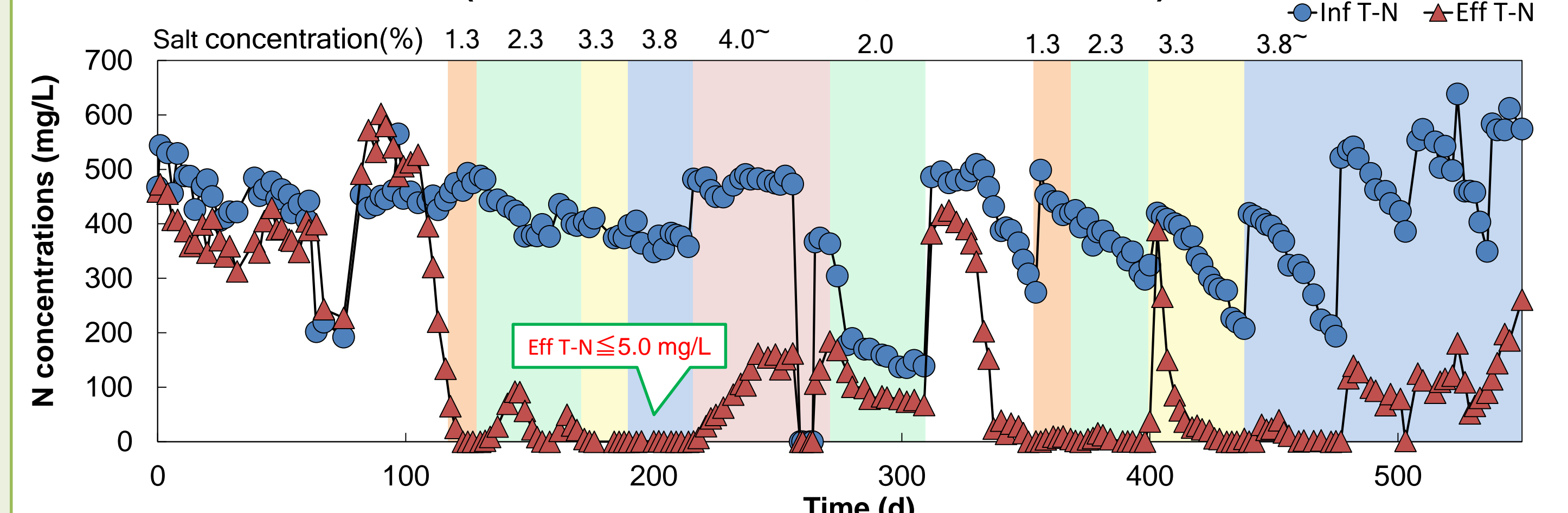


Fig.6 Total-N under different salt concentrations (RUN2:Entrapped method, Oxidic tank)

Table 2 Real-time PCR in the pellets (RUN1, Nitrification tank)

Target	copy number (copy/g)
<i>Nitrosomonas(amoA)</i>	2.02×10^9
<i>Nitrobacter(norB)</i>	9.62×10^9
<i>Nitrospira (16S rRNA)</i>	none

Conclusions

The maximum acceptable salt range by immobilized microgram using entrapped method (RUN1) and attached method (RUN2) were 3.8%.

Under 3.8% salt concentrations, RUN1 and RUN2 archived Eff T-N $<30 \text{ mg/L}$ in the industrial wastewater. Nitrification rate was obtained $0.4 \text{ kg/ kg-N/m}^3/\text{d}$.

Nitrification activity recovered under 0.3% salt concentration.